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Conference Proceedings:
CHEMICAL ENGINEERING JOURNAL (Elsevier)
CHEMICAL & ENGINEERING PROCESSING:
PROCESS INTENSIFICATION (Elsevier)

VP-9. Ivashkina E.N., Nurmakanova A.E., Boichenko S.S.
PROCESS PARAMETERS' INFLUENCE ON EFFICIENCY OF ALKYLATE COMPOSITION AND
OCTANE NUMBER

Tomsk Polytechnic University, Tomsk, Russia

VP-10. Kukueva V.V.

COMPUTATIONAL CHEMISTRY AS A TOOL FOR STUDYING OF THE PROCESSES IN THE CHEMICAL REACTORS ON THE MOLECULAR STAGES LEVEL

State Institution "Institute of Environmental Geochemistry" NAN Ukraine, Kiev, Ukraine

VP-11. Mityanina O.E., Samborskaya M.A.

OUTPUT MULTIPLICITY ANALYSIS OF METHYL TERT-BUTYL ETHER REACTIVE DISTILLATION SYNTHESIS

Tomsk Polytechnic University, Tomsk, Russia

VP-12. Nurmakanova A., Ivashkina E., Boychenko S.

ANALYSIS OF THE DEACTIVATION OF SULFURIC ACID DURING THE ALKYLATION OF ISOBUTANE WITH BUTENES

Tomsk Polytechnic University, Tomsk, Russia

VP-13. Pisarev M., Dolganov I., Dolganova I., Ivashkina E.

IMPROVING THE EFFICIENCY OF TECHNOLOGICAL GAS LOW-TEMPERATURE SEPARATION UNIT DEVICES USING SIMULATION DYNAMIC MODEL

Tomsk Polytechnic University, Tomsk, Russia

VP-14. Putin A.Y., Katsman E.A., Temkin O.N., Bruk L.G.

THE HYDROCARBOXYLATION OF ALKENES COUPLED WITH CARBON MONOOXIDE OXIDATION IN THE SYSTEM PdBr2-CuBr2-TETRAHYDROFURAN-H2O

Moscow Technological University, Moscow, Russia

VP-15. Sinitsin S.A., Petrov A.Yu., Nefedova N.V., Shulyaka S.E.

PROSPECTIVE FERRITE CATALYSTS FOR FLUE GASES CLEANING FROM CARBON MONOXIDE

D. Mendeleyev University of Chemical Technology of Russia, Moscow, Russia

VP-16. Tataurshchikov A.A., Ivanchina E., Krivtcova N.

APPLICATION OF INDUSTRIAL DATA OF LG-24/7 IN MODEL OF SULFUR COMPOUND KINETICS IN THE HYDROTREATING PROCESS

Tomsk Polytechnic University, Tomsk, Russia

VP-17. Tungatarova S., **Baizhumanova T.,** Zheksenbaeva Z., Abdukhalykov D., Zhumahok M. Kassumkan K.

Zhumabek M., Kassymkan K.

SILICON-TUNGSTEN HETEROPOLY COMPOUNDS - THE ACTIVE CATALYST COMPONENTS OF INCOMPLETE OXIDATIVE CONVERSION OF C_1 - C_2 ALKANES

D.V. Sokolsky Institute of Fuel, Catalysis and Electrochemistry, Almaty, Kazakhstan

VP-18. Tungatarova S., **Baizhumanova T.**, Zheksenbaeva Z., Zhumabek M., Kassymkan K. **CONVERSION OF LIGHT ALKANES INTO OXYGENATES**

D.V. Sokolsky Institute of Fuel, Catalysis and Electrochemistry, Almaty, Kazakhstan

VP-19. Tungatarova S., Baizhumanova T., Zhumabek M.

OXIDATION OF LIGHT ALKANES TO HYDROGEN-CONTAINING COMPOSITIONS OVER SUPPORTED BLOCK CATALYSTS

D.V. Sokolsky Institute of Fuel, Catalysis and Electrochemistry, Almaty, Kazakhstan

Conversion of Light Alkanes into Oxygenates

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Results of research the activity of polyoxide catalysts containing 1, 5 and 10% MoCrGa supported on natural carrier white clay (TWC) into oxidative conversion of propane-butane mixture into oxygenates are presented. The activity of developed catalysts (1% MoCrGa/TWC, 5% MoCrGa/TWC and 10% MoCrGa/TWC) in oxidation of reaction mixture to acetaldehyde, acetone and methyl ethyl ketone was investigated by varying the temperature from 673 to 823K and ratio of C_3 - C_4 : O_2 : N_2 : $Ar = 5: 1: 4: 5; \tau = 8$ s and GHSV = 450 h⁻¹. Studies have been done on a flow-type installation at atmospheric pressure in quartz tubular reactor with fixed catalyst bed. Analysis of initial substances and reaction products was carried out using chromatographic method on «Agilent Technologies 6890N».

Acetaldehyde was not formed on the 1% MoCrGa/TWC catalyst in the investigated temperature range. However, 33% acetaldehyde is formed on the 5% MoCrGa/TWC catalyst at 673K, the number of which gradually decreases with increasing of reaction temperature up to 12%. 36.5% acetaldehyde is formed on the 10% MoCrGa/TWC catalyst at 673K. The formation of acetaldehyde reached 40% while increasing the temperature to 723K, and reduced to 33% with a further increase in temperature.

Thus, 5% and 10% MoCrGa/TWC catalysts are optimal for the formation of acetaldehyde, on which is formed of 33% and 36.5% acetaldehyde at 673K, respectively.

Change in activity of studied catalysts by the formation of acetone was determined. Yield of acetone at all temperatures also does not observe on 1% MoCrGa/TWC catalyst. However, 33% acetone is formed on 5% MoCrGa/TWC catalyst at 673K, the amount of which increased to 50.9% with the growth of

temperature. 37% acetone is formed on 10% MoCrGa/TWC catalyst at 673K, but the number of acetone is reduced to a minimum with increasing temperature up to 823K.

Thus, the 5% MoCrGa/TWC is the optimal catalyst, on which the yield of acetone increased to 50.9% at 673-823K.

It was found that methyl ethyl ketone (MEK) is not formed on the 1% MoCrGa/TWC catalyst in reaction mixture. However, 20% MEK is formed on 5% MoCrGa/TWC catalyst at 673K, the amount of which increased to 38% with the growth of temperature. 15% MEK is formed on the 10% MoCrGa/TWC catalyst at 673K, but an inverse relationship in the formation of MEK is observed with increasing temperature up to 823K, the amount of which is reduced.

Thus, 5% MoCrGa/TWC catalyst is optimum for obtaining of 38% MEK, 50.9% acetone and 33% acetaldehyde.

Developed active catalysts can be the basis for the creation of a pilot utilization process of C_3 - C_4 hydrocarbons and production of oxygenates.

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